## Model Question Paper-1 with effect from 2019-20 (CBCS Scheme)

USN


# Fourth Semester B.E. Degree Examination <br> Stoichiometry 

TIME: 03 Hours
Max. Marks: 100
Note: 01. Answer any FIVE full questions, choosing at least ONE question from each MODULE.

| Module -1 |  |  | *Bloom's <br> Taxonomy Level | Marks |
| :---: | :---: | :---: | :---: | :---: |
| Q. 01 | a | The density of the liquid is $1500 \mathrm{~kg} / \mathrm{m}^{3}$. What is its specific gravity. What volume does 140 pounds of this material will occupy? | L1,L2 | 06 |
|  | b | $\mathrm{AgNO}_{3}$ reacts with $\mathrm{BaCl}_{2}$ to form $\mathrm{AgCl} \& \mathrm{Ba}\left(\mathrm{NO}_{3}\right)_{2}$ <br> i. Write the balanced chemical equation <br> ii. If 39.02 g of $\mathrm{BaCl}_{2}$ reacted in an excess of $\mathrm{AgNO}_{3}$, how many representative particles of AgCl are produced. <br> iii. If 40 g of $\mathrm{Ba}\left(\mathrm{NO}_{3}\right)_{2}$ are produced how many grams of $\mathrm{AgNO}_{3}$ were reacted | L2,L3 | 14 |
| OR |  |  |  |  |
| Q. 02 | a | A product gas from a reaction has the composition by weight. $\mathrm{Cl}_{2}-67 \%$, $\mathrm{Br}_{2}-28 \%, \mathrm{O}_{2}-5 \%$, using the ideal gas law calculate <br> i. the composition of gas by volume <br> ii. the density of the mixture in $\mathrm{g} / \mathrm{L}$ at $25^{\circ} \mathrm{C}$ <br> iii. Specific gravity of the mixture. <br> iv. Average molecular weight of the mixture. | L2,L3 | 08 |
|  | b | A compound whose molecular weight is 103, analyses C-81.5\%, H2$4.9 \%$ and $\mathrm{N} 2-13.6 \%$. What is its molecular formula? | L2,L3 | 08 |
|  | c | What is the molarity of a solution containing 8 g of EDTA in $300 \mathrm{~cm}^{3}$ of it? | L2,L3 | 04 |
| Module-2 |  |  |  |  |
| Q. 03 | a | Feed containing $50 \%$ of benzene and $50 \%$ of toluene is fed to the distillation column at a rate of $5,000 \mathrm{~kg} / \mathrm{hr}$. Distillate contains $95 \%$ benzene and bottom product contains $92 \%$ toluene. All percentages are by weight percentage. <br> I. Calculate the mass flow rate of distillate and bottom product \% Recovery of Benzene | L2,L3 | 10 |
|  | b | 2000 kg of wet solids by weight containing $70 \%$ solid by weight are fed to a tray drier and is dried by hot air.The product finally obtained is found to contain $1 \%$ moisture and $99 \%$ solids by weight. <br> Calculate i) kg of water removed from wet solids <br> ii) kg of product obtained | L2,L3 | 10 |
| OR |  |  |  |  |
| Q. 04 | a | A liquid adhesive, which is used to make laminated boards, consists of a polymerdissolved in a solvent. The amount of polymer in the solution has to be carefully controlled for this application. When the supplier of the adhesive receives an order for 3000 kg of an adhesivesolution containing $13 \mathrm{wt} \%$ polymer, all it has on hand is (1) 500 kg of a $10 \mathrm{wt} \%$ solution, (2) avery large quantity of a $20 \mathrm{wt} \%$ solution, and (3) pure solvent. Calculate the weight of each of the three stocks that must be blended together to fill the order. | L2,L3 | 12 |


|  | b | A single effect evaporator is fed with $10000 \mathrm{~kg} / \mathrm{h}$ of weak liquor containing $15 \%$ caustic by weight and is concentrated to get thick liquor containing $40 \%$ by weight caustic. Calculate: <br> (a) $\mathrm{kg} / \mathrm{h}$ of water evaporated and <br> (b) $\mathrm{kg} / \mathrm{h}$ of thick liquor |  |  |  |  | L2,L3 | 08 |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| Module-3 |  |  |  |  |  |  |  |  |
| Q. 05 | a | Explain the importance of recycle and bypass using block diagram. |  |  |  |  | L1,L2 | 08 |
|  | b | Fresh juice contains $12 \%$ solids \& the rest water. It is concentrated to contain $42 \%$ solids. The evaporator is bypassed with a fraction of fresh juice. Juice that enters the evaporator is concentrated to $58 \%$ solids and is mixed with bypassed juice to achieve the desired concentration. Calculate the amount of concentrated juice per kg of fresh juice. |  |  |  |  | L2,L3 | 12 |
| OR |  |  |  |  |  |  |  |  |
| Q. 06 | a | The gross heating value of gaseous propane $\left(\mathrm{C}_{3} \mathrm{H}_{8}\right.$ at 298 K is $2219.5 \mathrm{~kJ} / \mathrm{mol}$. Calculate its net heating value considering latent heat of water vapour at 298 K is $2442.5 \mathrm{~kJ} / \mathrm{kg}$ obtain the amount of water from reduction. |  |  |  |  | L1,L2,L3 | 08 |
|  | b | Write a not | on types an | aracteristic | of fuels | d biofuels | L1,L2 | 12 |
| Module-4 |  |  |  |  |  |  |  |  |
| Q. 07 | a | Define the following <br> i) Heat of reaction ii) Heat of formation iii) Heat of combustion |  |  |  |  | L1,L2 | 03 |
|  | b | The temperature of $\mathrm{O}_{2}$ is raised from 350 K to 1500 K . Calculate the amount of heat that must be supplied for raising the temperature of 1 kmol of $\mathrm{O}_{2}$ using $\mathrm{C}_{\mathrm{p}}$ data given. $\mathrm{Cp}=26.0257+11.7551 \times 10^{-3} \mathrm{~T}-2.3426 \times 10^{-6} \mathrm{~T}^{2}-$ $0.5623 \times 10^{-9} \mathrm{~T}^{3} \mathrm{~kJ} / \mathrm{mol} \mathrm{K}$. |  |  |  |  | L2,L3 | 10 |
|  | c | Calculate the heat of formation of methane gas from the following heat of combustion data.$\begin{array}{lll} \mathrm{CH}_{4}(\mathrm{~g})+2 \mathrm{O}_{2}(\mathrm{~g}) & \mathrm{C@}_{2}(\mathrm{~g})+2 \mathrm{H}_{2} \mathrm{O} & (\mathrm{l}) \Delta \mathrm{H}_{298}=-890.94 \mathrm{~kJ} \\ \mathrm{C}(\mathrm{~g})+\mathrm{O}_{2}(\mathrm{~g}) & \mathrm{CO}_{2}(\mathrm{~g}) & \Delta \mathrm{H}_{298}=-393.78 \mathrm{~kJ} \\ \mathrm{H}_{2}(\mathrm{~g})+1 / 2 \mathrm{O}_{2}\left(\mathrm{~g} \longrightarrow \longrightarrow \mathrm{H}_{2} \mathrm{O}(\mathrm{l})\right. & \Delta \mathrm{H}_{298}=-286.03 \mathrm{~kJ} \end{array}$ |  |  |  |  | L2,L3 | 07 |
| Q 08 OR |  |  |  |  |  |  |  |  |
| Q. 08 | a | A stream flowing at a rate of $15000 \mathrm{~mol} / \mathrm{hr}$ containing $25 \mathrm{~mol} \% \mathrm{~N}_{2}$ and 75 $\mathrm{mol} \% \mathrm{H}_{2}$ is to be heated from 298 K to 473 K . Calculate the that must be transferred using Cp data given below, $\mathrm{Cp}=\mathrm{a}+\mathrm{bT}+\mathrm{cT}^{2}+\mathrm{dT}^{3} \mathrm{~kJ} / \mathrm{mol} \mathrm{K}$ |  |  |  |  | L2,L3 | 10 |
|  | b | Calculate the standard heat of formation of $n$-propanol liquid using the following data: <br> Standard heat of formation of $\mathrm{CO}_{2}(\mathrm{~g})=-393.51 \mathrm{~kJ} / \mathrm{mol}$ <br> Standard heat of formation of $\mathrm{H}_{2} \mathrm{O}=-285.83 \mathrm{~kJ} / \mathrm{mol}$ <br> Standard heat of Combustion of n-propanol $\left[\mathrm{C}_{3} \mathrm{H}_{7} \mathrm{OH}\right](\mathrm{l})=-2028.19 \mathrm{~kJ} / \mathrm{mol}$ |  |  |  |  | L2,L3 | 10 |
| Module-5 |  |  |  |  |  |  |  |  |
| Q. 09 | a | Explain the different downstream process involved in production of Ethanol. |  |  |  |  | L1,L2 | 10 |
|  | b | Write a note on development of bioprocess technology. |  |  |  |  | L1,L2 | 10 |
| OR |  |  |  |  |  |  |  |  |
| Q. 10 | a | Explain with an example, the process flow sheet and unit operations involved in bioprocess industry. |  |  |  |  | L1,L2 | 10 |
|  | b | Explain the different downstream process involved in production of Pencillin. |  |  |  |  | L1,L2 | 10 |

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[^0]:    *Bloom's Taxonomy Level: Indicate as L1, L2, L3, L4, etc. It is also desirable to indicate the COs and POs to be attained by every bit of questions.

